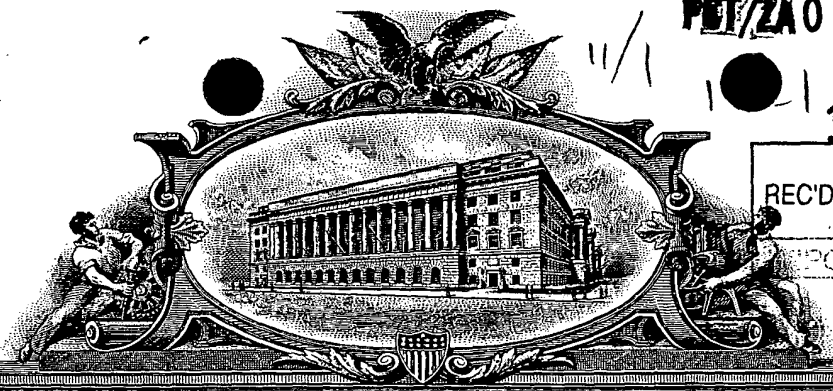


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PROVISIONAL APPLICATION COVER SHEET

07/06/99
Jc648 U.S. PRO
60/142381

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This is a request for filing a PROVISIONAL APPLICATION under 37 CFR 1.53(c).

DOCKET NO.		F 217		TYPE A PLUS SIGN (+) INSIDE THIS BOX →		+	
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TITLE OF THE INVENTION (280 characters max)							
METATHESIS OF FISCHER-TROPSCH PROCESS PRODUCTS TO PRODUCE ALKYL BENZENES, DRILLING FLUIDS AND OXO-ALCOHOLS							
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STATE	VA		ZIP CODE	22202		COUNTRY	USA
ENCLOSED APPLICATIONS PARTS (check all that apply)							
X	Specifica- tion	No. of Pages	10	Small Entity Statement			
	Drawing(s)	No. of Sheets					
METHOD OF PAYMENT (check one)							
X	A check in the amount of \$150 to cover the filing fee is enclosed.			Check No. 14490		PROVISIONAL FILING FEE	\$150
X	The Commissioner is hereby authorized to charge the filing fee and credit Deposit Account No.:			25-0120			

☒ Additional inventors are being named on separately numbered sheets attached hereto.

The invention was made by an agency of the United States Government or under a contract with an agency of the United States Government.

☒ No.

☐ Yes, the name of the U.S. Government agency and the Government contract number are:

Respectfully submitted,

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PROVISIONAL APPLICATION FILING ONLY

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669070-TECHTOS

**METATHESIS OF FISCHER-TROPSCH PROCESS PRODUCTS TO
PRODUCE ALKYL BENZENES, DRILLING FLUIDS AND OXO-ALCOHOLS**

The invention provides alkyl benzene (AB), drilling fluid and oxo-alcohols derived from metathesis of Fischer-Tropsch process products.

Conversion of lower olefins to higher olefins can be achieved by an isomerizing metathesis process, or metathetic oligomerisation. Conventional metathesis processes require an olefinic feedstock high in purity and linearity and produce highly linear products.

Various heterogeneous contact catalysts such as $\text{Re}_2\text{O}_7/\text{Al}_2\text{O}_3$ and $\text{Re}_2\text{O}_7/\text{Al}_2\text{O}_3.\text{SiO}_2$, and also combinations of these catalysts with co-catalysts can be used for metathesis of unfunctionalized olefins. However, other catalyst and co-catalyst combinations, for example for homogeneous metathesis using WCl_6 and/or ReCl_6 and a co-catalyst, have been used successfully and the invention is not limited to any specific catalyst system, nor to homogeneous or heterogeneous metathesis.

Surprisingly, and contrary to conventional thinking, it has now been found that by using metathesis on Fischer-Tropsch process products i.e. using Fischer-Tropsch feedstock to the metathesis process, which feedstock includes both branched and unbranched olefins, as well as non-olefinic components, specific hydrocarbons having between 8 and 18 carbons can be obtained, which hydrocarbons may be used to derive AB, oxo-alcohols and drilling fluid.

By a Fischer-Tropsch process product or feedstock is meant a product obtained by subjecting a synthesis gas including carbon monoxide and hydrogen, to Fischer-Tropsch reaction conditions in the presence of typically an iron based catalyst, a cobalt based catalyst, and iron/cobalt based catalyst, or any other Fischer-Tropsch catalyst, under Fischer-Tropsch reaction conditions.

This invention provides products in the 8 to 18 carbon range derived from 5 to 10 carbon Fischer-Tropsch process products, the products in the 8 to 18 carbon range having a desirable degree of branching or non-linearity.

Thus, according to a first aspect of the invention, there is provided an oxo-alcohol composition including oxo-alcohols having between 8 and 18 carbon atoms, the oxo-alcohols being derived from olefins obtained by metathesis of one or more of 5, 6, 7, 8, 9 and/or 10 carbon containing Fischer-Tropsch derived feedstock.

Between 10% and 90% of the oxo-alcohols of the composition may be branched oxo-alcohols.

5 The oxo-alcohols of the composition may be predominantly linear, with between 10% and 49% branched oxo-alcohols in the composition.

The composition includes between 15% and 35% branched oxo-alcohols.

10

The composition includes 24% branched oxo-alcohols.

The branching on the branched oxo-alcohols is predominantly mono-methyl branching, however, some di-methyl branching may also be present.

15

Typically, the mono-methyl branching will be in excess of 90% of the branching, or even in excess of 95%.

20 Typically, the oxo-alcohols of the composition in the 8 to 10 carbon range are usable as plasticizer alcohols.

Typically, the oxo-alcohols of the composition in the 10 to 16 carbon range are usable as detergent alcohols.

A typical product make up from the metathesis of a 7 carbon Fischer-Tropsch derived feedstock and suitable for deriving oxo-alcohols therefrom is set out in Table 1 at the end of the specification.

5 This product of Table 1 may typically be hydroformylated using a Co-EP catalyst, or any other suitable catalyst, to form predominantly linear alcohols, the ratio of linear to branched alcohols being related to the ratio of linear to branched product of the metathesis of the 7 carbon Fischer-Tropsch derived feedstock.

10

Thus, according to a second aspect of the invention, there is provided an alkyl benzene (AB) composition including AB having between 10 and 14 carbon atoms on the alkyl chain, the AB being derived from olefins obtained by metathesis of one or more of a 6,7 and/or 8 carbon containing Fischer-Tropsch derived feedstock.

15

The AB composition may contain between 10% and 90% of branched alkyl chain AB.

20

The AB composition may contain predominantly linear alkyl chain AB, with between 10% and 49% branched alkyl chain AB in the composition.

The composition includes between 15% and 35% branched alkyl chain AB.

The composition includes about 24% branched alkyl chain AB.

The branching on the branched alkyl chain of the AB is predominantly
5 mono-methyl branching, however, some di-methyl, ethyl, and /or propyl
branching may also be present.

Typically, the mono-methyl branching will be in excess of 90% of the
branching, or even in excess of 95%.

A typical AB product make up produced from the products of
metathesis of a 9 carbon Fischer-Tropsch derived feedstock is set out in
Table 3 at the end of the specification.

The AB may be sulfonated to give an alkyl benzene sulfonate which
15 may be used as a detergent. However, the AB composition itself may have
uses such as for drilling fluids.

The product of Table 3 was fractionated and a 10 to 14 carbon alkyl
20 chain AB fraction was obtained having the following composition (represented
as the linear internal olefin only):

Dec nes : 16.53%
Undecenes : 27.96%
Dodecenes : 26.19%
Tridecenes : 4.71%
3 Tetradecenes: 0.91%

Methyl branched internal olefins in the 10 to 14 carbon range make up most of the remainder.

Thus, according to a third aspect of the invention, there is provided a drilling fluid composition including hydrocarbons having between 14 and 18 carbon atoms, the hydrocarbons being derived from olefins obtained by metathesis of one or more of a 8, 9 and/or 10 carbon containing Fischer-Tropsch derived feedstock.

The drilling fluid composition may include between 10% and 90% branched hydrocarbons.

The hydrocarbons of the drilling fluid composition may be predominantly linear, with between 10% and 49% branched hydrocarbons in the composition.

The composition includes between 15% and 35% branched hydrocarbons.

The composition includes about 24% branched hydrocarbons.

The branching on the branched hydrocarbons is predominantly mono-
5 methyl branching, however, some di-methyl, ethyl, and/or propyl branching
may also be present.

Typically, the mono-methyl branching will be in excess of 90% of the
branching, or even in excess of 95%.

A typical product make up from the metathesis of a 9 carbon Fischer-
Tropsch derived feedstock and suitable for deriving the drilling fluid
composition is set out in Table 2 at the end of the specification.

The product of Table 2 was fractionated and a 14 to 17 carbon fraction
was obtained having the following approximate composition (represented as
both methyl branched and linear internal olefins):

	Tetradecenes	:	23.03%
20	Pentadecenes	:	38.40%
	Hexadecenes	:	36.22%
	Heptadecene	:	2.35%

TABLE 1: Mass and component balance : Batch distillation of water washed SLO C7 cut

MASS CATALYST (g) 51.81
 MASS C7 FEED (g) 316.38
 MASS PRODUCT (g) 280.55
 mol m-xylenes + n-heptenes in 2.90
 mol m-xylenes + n-heptenes out 0.26
 heptene conversion 91.05
 mol C10-14 formed 0.94
 mol % yield 65.18
 selectivity (%) 71.58

COMPONENT	FEED		FEED		From GC		normalized		mass L		mass G/L		mass%	
	mass %	mass (g)	moles	FEED	mass %	moles	mass %	moles	mass	moles	mass	moles	mass%	moles%
3-Methyl-hexane	1.0553	3.3331	0.0345		0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
5-Methyl-hexane	2.3555	7.4640	0.0762		0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
4-Methyl-hexane	3.8128	12.0632	0.1228		0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
2-Methyl-hexane	6.0078	19.0076	0.1928		0.2708	0.2890	0.2890	0.0000	0.8109	0.0000	0.8109	0.0000	0.2828	0.0000
2-Methylheptane	1.8820	5.9357	0.0534		2.3491	2.4352	2.4352	0.0000	6.8320	0.0592	6.8320	0.0592	2.0457	0.0000
3-Methylheptane	3.0273	9.5777	0.0956		3.8165	3.9564	3.9564	0.0000	11.0985	0.1108	11.0985	0.1108	3.3236	0.0000
1-heptene	75.6071	238.4580	2.4397		1.1195	1.1594	1.1594	0.0000	3.2528	0.0331	3.2528	0.0331	0.9740	0.0000
n-heptane	2.5700	8.1311	0.0811		2.7408	2.8411	2.8411	0.0000	7.9706	0.0796	7.9706	0.0796	2.3887	0.0000
heptene (2,E)	0.0000	0.0000	0.0000		0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
3-Heptene	0.9803	3.1018	0.0316		3.5837	3.7150	3.7150	0.0000	10.4226	0.1051	10.4226	0.1051	3.1209	0.0000
diene or cyclic olefin	1.0121	3.2020	0.0359		0.0909	0.0942	0.0942	0.0000	0.2643	0.0027	0.2643	0.0027	0.0791	0.0000
2-Heptene	0.0000	0.0000	0.0000		3.7687	3.9069	3.9069	0.0000	10.9507	0.1118	10.9507	0.1118	3.2620	0.0000
Diene or cyclic olefin	0.5084	1.6115	0.0168		0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Ellylene					0.0392	0.0408	0.0408	0.0000	0.2385	0.2385	0.2385	0.2385	1.5997	0.0000
Propylene					0.8708	0.9027	0.9027	0.0000	2.2708	0.2196	2.2708	0.2196	3.4060	0.0000
Butenes					1.2848	1.3111	1.3111	0.0000	3.2950	0.2196	3.2950	0.2196	3.6818	0.0000
Pentenes					3.0284	3.1405	3.1405	0.0000	7.9706	0.1977	7.9706	0.1977	4.1432	0.0000
Hexenes					1.5405	1.6001	1.6001	0.0000	4.4891	0.2900	4.4891	0.2900	7.2954	0.0000
methyl branched heptenes					11.1916	11.6018	11.6018	0.0000	32.5489	0.2900	32.5489	0.2900	1.3442	0.0000
n-octenes					6.5000	6.8944	6.8944	0.0000	24.9533	0.1977	24.9533	0.1977	8.7463	0.0000
n-Nonenes					1.5263	1.5859	1.5859	0.0000	4.7299	0.0337	4.7299	0.0337	7.4719	0.0000
methyl branched nonenes					10.5892	10.9773	10.9773	0.0000	30.7969	0.2196	30.7969	0.2196	1.4163	0.0000
n-Decenes					3.1152	3.2305	3.2305	0.0000	9.0530	0.0587	9.0530	0.0587	9.2216	0.0000
methyl branched decenes					14.3685	14.8951	14.8951	0.0000	41.7883	0.2708	41.7883	0.2708	12.5128	0.0000
n-undecenes					2.6538	2.7814	2.7814	0.0000	7.7472	0.0460	7.7472	0.0460	2.3199	0.0000
methyl branched undecenes					13.8046	14.3106	14.3106	0.0000	40.1483	0.2385	40.1483	0.2385	12.0218	0.0000
n-dodecenes					0.4917	0.5097	0.5097	0.0000	1.4301	0.0079	1.4301	0.0079	0.4282	0.0000
methyl branched dodecenes					3.9527	3.4860	3.4860	0.0000	9.7789	0.0536	9.7789	0.0536	2.9284	0.0000
tridecenes					0.8584	0.8899	0.8899	0.0000	2.4956	0.0127	2.4956	0.0127	0.7476	0.0000
pentadecene					0.1911	0.1981	0.1981	0.0000	0.5558	0.0026	0.5558	0.0026	0.1664	0.0000
unknowns	1.2855	4.0007												
heavier					1.1257	1.1670	1.1670	0.0000	3.2739	0.2385	3.2739	0.2385	0.9803	0.0000
TOTAL	100.0000	316.3800	3.1638		100.0000	3.1638	100.0000	3.1638	316.3800	3.1638	316.3800	3.1638	100.0000	100.0000

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TABLE 2: Mass and component balance

3) Batch Meth reaction of isobutylene with SLO C9 cat (MS40 treated)

C9 / Re207	1000.1
MASS CATALYST (g)	0.75
MASS C9 FEED (g)	10.71
MASS PRODUCT (g)	8.99
mol n-octanes + n-nonanes in	0.07
mol n-octanes + n-nonanes out	0.01
monomer conversion	80.56
mol C14-16 formed	0.02
mol % yield	52.28
selectivity (%)	64.90

COMPONENT	FEED mass %	FEED mass (g)	FEED molar %	FROM GC PRODUCT mass %	normalized PRODUCT molar %	mass PRODUCT molar %	mass PRODUCT molar %	mass PRODUCT molar %
3-Methyl-octane	0.1407	0.151	0.0001	0.0000	0.0000	0.0000	0.0000	0.0000
7-Methyl-octane	0.0008	0.1050	0.0008	0.0000	0.0000	0.0000	0.0000	0.0000
6-Methyl-octane	0.0037	0.1002	0.0008	0.0000	0.0000	0.0000	0.0000	0.0000
2-Methyl-octane	0.0002	0.0083	0.0008	0.0000	0.0000	0.0000	0.0000	0.0000
4-Methyl-octane	1.1457	0.1228	0.0010	1.8315	1.5620	0.1960	0.0012	0.1960
3-Methyl-octane	1.5031	0.1616	0.0013	1.8553	1.9441	0.1941	0.0015	0.1941
n-nonanes	75.5614	8.0890	0.0641	15.6354	16.3747	1.6350	0.0130	1.6350
n-nonane	11.3149	1.2113	0.0121	13.5302	14.1700	1.4149	0.0110	1.4149
dimethylcyclohexane	1.7378	0.1960	0.0019	1.1309	1.1043	0.1183	0.0008	0.1183
ethylcyclohexane				0.7247	0.7390	0.0065	0.0001	0.0065
propylene				1.0477	1.0572	0.0041	0.0001	0.0041
butadiene				0.4504	0.4622	0.0021	0.0001	0.0021
pentadiene				0.2503	0.3071	0.0010	0.0001	0.0010
hexadiene				1.4233	1.4227	0.0015	0.0001	0.0015
heptadiene				4.5070	4.7202	0.0042	0.0004	0.0042
n-octanes				10.3012	10.7883	0.0172	0.0077	0.0172
n-octane				1.8046	1.8039	0.1967	0.0012	0.1967
n-decenes				1.5563	1.6716	0.1689	0.0010	0.1689
n-decane				3.5788	3.7480	0.3742	0.0021	0.3742
undecenes				0.0000	0.0000	0.0000	0.0000	0.0000
undecane				7.6190	7.9789	0.7967	0.0041	0.7967
dimethyl branched C13				0.6949	0.7277	0.0727	0.0004	0.0727
trimethyl branched C14				13.1270	13.7477	1.3727	0.0085	1.3727
pentamethyl branched C15				0.7346	0.7683	0.0768	0.0004	0.0768
hexamethyl branched C16				13.0782	13.6946	1.3674	0.0061	1.3674
heptamethyl branched C17				0.9497	0.9898	0.0988	0.0004	0.0988
unknowns	5.7457	0.6151		4.5151	0.0000	0.0000		
TOTAL	94.2543	10.7052	0.0608	85.6449	100.0000	9.7208	0.0650	100.0000

TABLE 3: P ak Assignments and Mass %

Summary

Assignment	Mass%
Branched C ₁₀ benzene	0.61
Branched C ₁₀ benzene	0.12
Branched C ₁₀ benzene	0.14
Branched C ₁₀ benzene	0.20
Branched C ₁₀ benzene	0.29
Branched C ₁₀ benzene	0.39
5-Decylbenzene	2.91
4-Decylbenzene	2.79
Branched C ₁₀ benzene	0.17
Branched C ₁₀ benzene	0.70
3-Decylbenzene	4.34
Branched C ₁₀ benzene	0.25
Branched C ₁₀ benzene	0.82
Branched C ₁₁ benzene	1.23
2-Decylbenzene	5.67
Branched C ₁₁ benzene	0.70
Branched C ₁₁ benzene	0.57
Branched C ₁₁ benzene	0.88
5+6-Undecylbenzene	7.85
Branched C ₁₁ benzene	0.52
4-Undecylbenzene	4.59
Branched C ₁₁ benzene	1.78
3-Undecylbenzene	8.48
Branched C ₁₁ benzene	1.10
Branched C ₁₂ benzene	0.41
Branched C ₁₂ benzene	0.63
2-Undecylbenzene	10.22
Branched C ₁₂ benzene	0.59
Branched C ₁₂ benzene	0.94
8-Dodecylbenzene	4.57
5-Dodecylbenzene	3.83
Branched C ₁₂ benzene	0.71
4-Dodecylbenzene	3.85
Branched C ₁₂ benzene	0.49
Branched C ₁₂ benzene	0.54
Branched C ₁₂ benzene	0.82
3-Dodecylbenzene	5.98
Branched C ₁₂ benzene	0.66
Branched C ₁₃ benzene	0.74
2-Dodecylbenzene	7.92
5+6-Tridecylbenzene	1.04
4-Tridecylbenzene	0.73
3-Tridecylbenzene	1.42
2-Tridecylbenzene	1.38
Branched C ₁₄ Benzenes	0.48
Branched C ₁₄ Benzenes	1.45
5+6-Tetradecylbenzene	0.50
4-Tetradecylbenzene	0.21
3-Tetradecylbenzene	0.51
2-Tetradecylbenzene	0.77
Total	100.00

C ₁₀	
2-Decylbenzene	6.67
3-Decylbenzene	4.34
4-Decylbenzene	2.79
5-Decylbenzene	2.91
Total linear	16.90
Total branched	3.65
Total	20.55
C ₁₁	
2-Undecylbenzene	10.22
3-Undecylbenzene	8.48
4-Undecylbenzene	4.59
5+6-Undecylbenzene	7.85
Total linear	31.28
Total branched	6.78
Total	38.04
C ₁₂	
2-Dodecylbenzene	7.92
3-Dodecylbenzene	5.98
4-Dodecylbenzene	3.85
5-Dodecylbenzene	3.83
6-Dodecylbenzene	4.57
Total linear	26.13
Total branched	6.05
Total	32.21
C ₁₃	
2-Tridecylbenzene	1.38
3-Tridecylbenzene	1.42
4-Tridecylbenzene	0.73
5+6-Tridecylbenzene	1.04
Total linear	4.58
Total branched	0.74
Total	5.30
C ₁₄	
2-Tetradecylbenzene	0.77
3-Tetradecylbenzene	0.51
4-Tetradecylbenzene	0.21
5+6-Tetradecylbenzene	0.50
Total linear	1.98
Total branched	1.91
Total	3.90
Total LAB	100.00

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